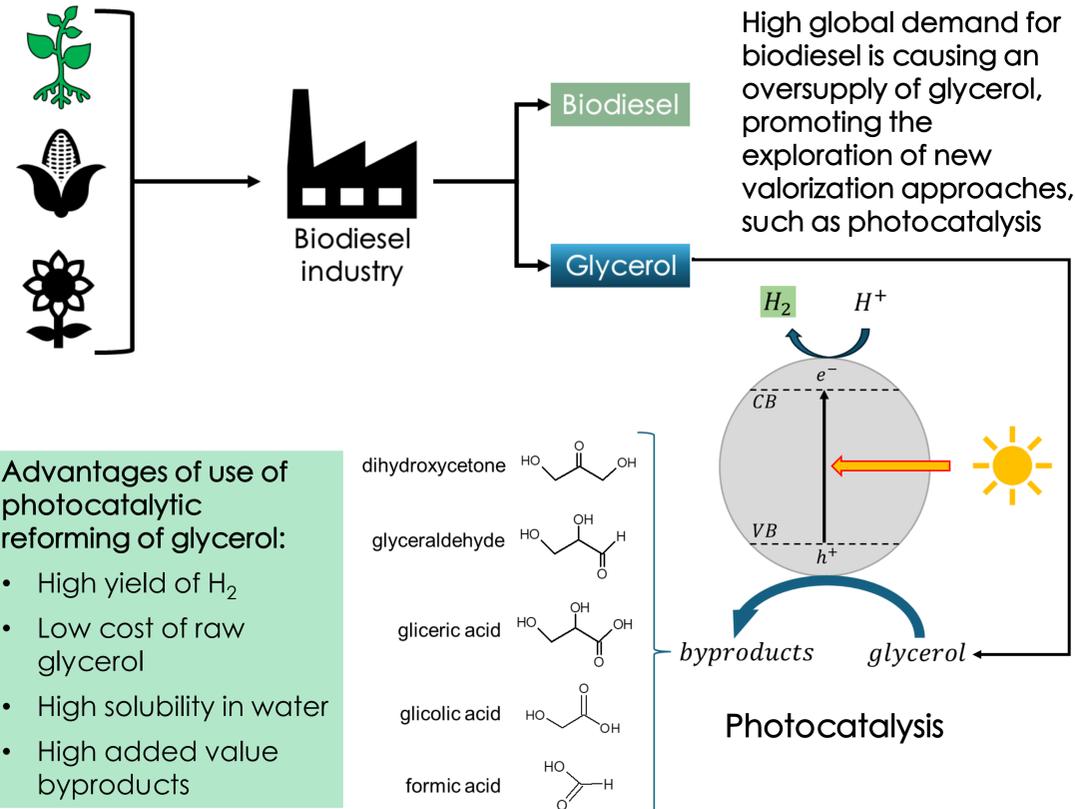
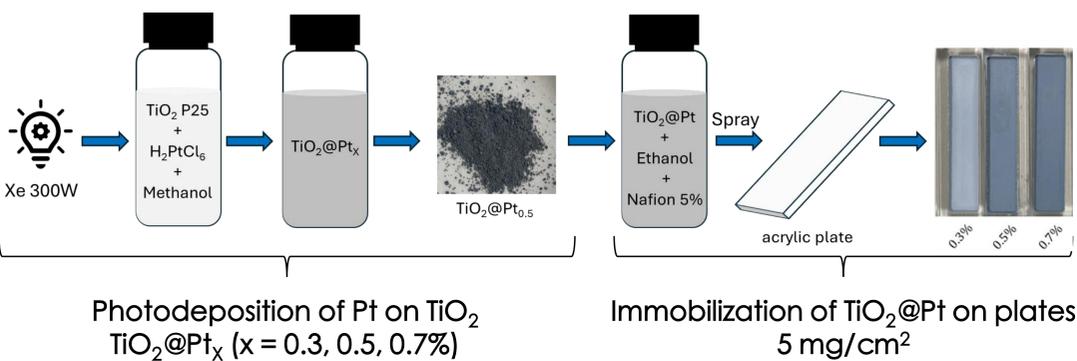


INTRODUCTION

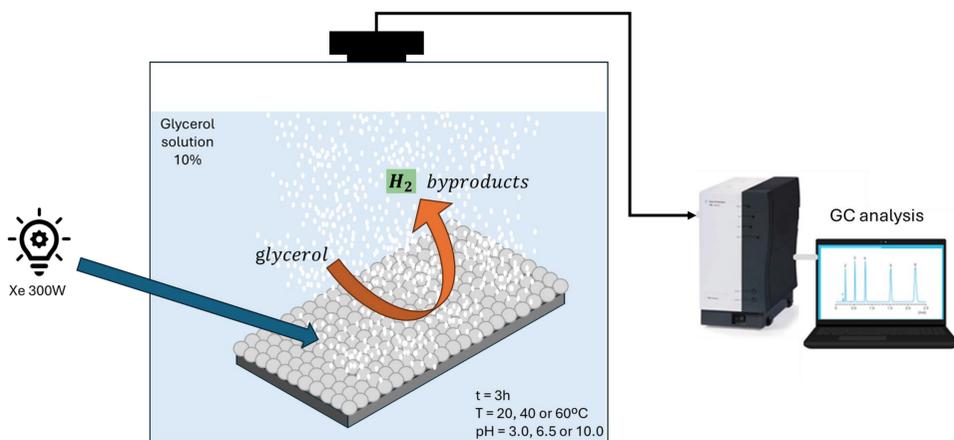


EXPERIMENTAL

Synthesis of photocatalyst and immobilization on glass plate



Photocatalytic reaction



RESULTS

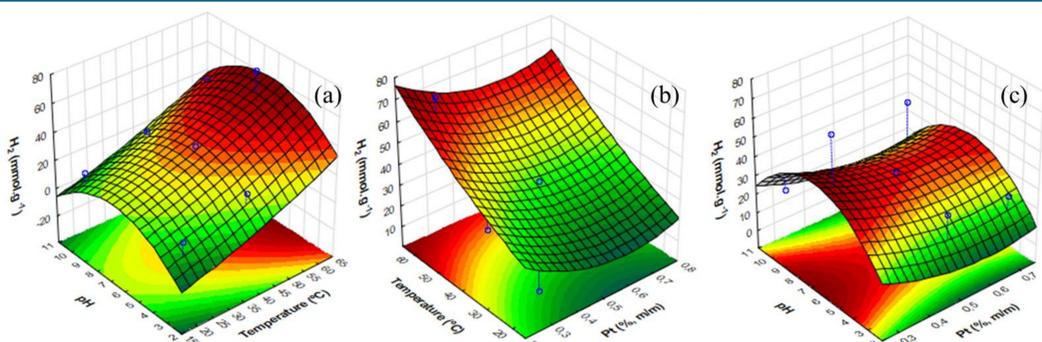


Fig. 1. Response surface of photocatalytic H₂ production. Glycerol: 10% (v/v). Catalyst: 0.4 g/L. t = 3h.

Photocatalytic performance

Evaluation of the variables of the photocatalytic process in the H₂ production

| Pt (% m/m) | Temperature (°C) | pH | H ₂ (mmol.g ⁻¹) |
|------------|------------------|------|--|
| 0.3 | 20 | 3.0 | 11.82 |
| 0.3 | 40 | 10.0 | 23.63 |
| 0.3 | 60 | 6.5 | 69.90 |
| 0.5 | 20 | 10.0 | 13.13 |
| 0.5 | 40 | 6.5 | 35.45 |
| 0.5 | 60 | 3.0 | 30.86 |
| 0.7 | 20 | 6.5 | 13.79 |
| 0.7 | 40 | 3.0 | 24.95 |
| 0.7 | 60 | 10.0 | 42.02 |

Glycerol: 10% (v/v). Catalyst: 0.4 g/L. t = 3h.

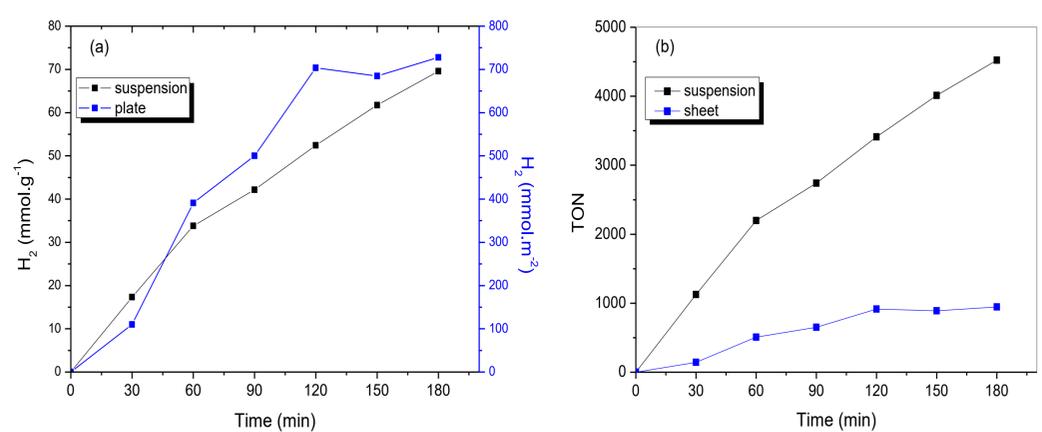


Fig. 2. (a) Profile of photocatalytic hydrogen production and (b) TON, with application of the catalyst in suspension and immobilized on a plate. Glycerol: 10% (v/v), Pt = 0.3% (m/m), temperature: 60°C.

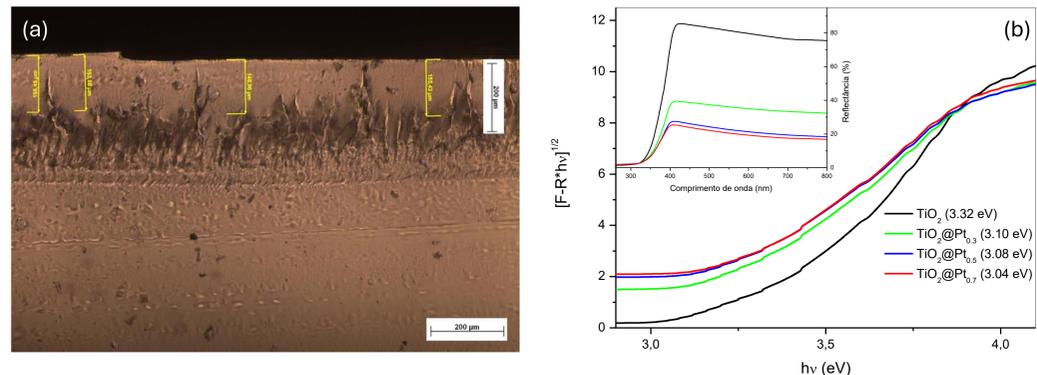


Fig. 3. (a) Microscopy image of thickness and (b) diffuse reflectance profiles of TiO₂@Pt_x catalysts (x = 0.3, 0.5 and 0.7%)

CONCLUSIONS

The optimization of process variables revealed that temperature was the most relevant factor for hydrogen production. Furthermore, it was observed that a pH condition close to neutrality was favorable to the photocatalytic process

The catalysts in suspension and immobilized on plates showed similar results. However, the catalyst dispersed in powder demonstrated a more constant and continuous production profile.

The results suggest that immobilizing the catalyst on plates can provide a scalable solution for the photocatalytic process, minimizing costs and time associated with applying the catalyst in powder form.

ACKNOWLEDGMENTS